

Optimizing Thermal Processes in Waterspray Retorts

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Why Optimize a Thermal Process?

- Reduce cycle time
 - Eliminate retorts as bottleneck
 - Increase throughput
 - Reduce overhead cost per case
- Quality Improvement
- Reduce utility costs

Optimization Considerations

- Product
 - Conductive vs. Convective Heating
- Package
 - Rigid, semi-rigid, or flexible
 - Pressure profile to maintain container integrity
- Steam Supply
- Cooling Water
 - Seasonal water temperature
 - Recirculation systems
 - Chillers

Optimization Focus

- Rotation
 - Determine optimal rate for heat transfer and product quality
- Heating
 - Come-up temperature profile
 - Come-up overpressure profile
- Cooling
 - Cooling temperature profile
 - Cooling pressure profile

Optimization Focus: Rotation

During process development, the optimal rotation rate should be determined with consideration to finding a balance between:

1. Product heating rate
2. Product quality
3. Retort mechanical reliability

Optimization Focus: Heating

Typically, come-up profiles rely on the steam pressure being delivered to the retort.

The following example demonstrates how increasing the steam pressure from 80 to 100 psi can reduce the cycle time by reducing the come-up time.

(Target $F_0 = 6.0$ at the end of heating)

Normal 12' CUT

NumeriCAL Process Calculation

PRODUCT IDENTIFICATION | PROCESS DATA

z-Value: Reference Temp: Initial Temp: Temp Unit: Simple or Broken:
 Evaluation: Container Type: Container Dimension: Today:

Segments	1S	2S	3S	4S	5C	6C	7C	8C	9C
Duration (min)	4.00	4.00	4.00	72.67	2.00	10.00	10.00	5.00	30.00
RT Begin	70.00	200.00	235.00	250.00	250.00	240.00	200.00	140.00	70.00
RT End	200.00	235.00	250.00	250.00	240.00	200.00	140.00	70.00	70.00
jh or jc	1.91	1.91	1.91	1.91	1.56	1.56	1.56	1.56	1.56
fh, f2, f3 or fc	48.21	48.21	48.21	48.21	53.26	53.26	53.26	53.26	53.26
Elapsed Time	4.00	8.00	12.00	84.67	86.67	96.67	106.67	111.67	141.67
Retort Temp	200.00	235.00	250.00	250.00	240.00	200.00	140.00	70.00	70.00
Product Temp	90.00	90.72	95.65	243.37	243.82	243.09	231.61	220.57	120.37
Accum F Value	0.000	0.000	0.000	6.060	6.944	11.648	14.097	14.356	14.412

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OK Cancel Apply

CUT Reduced to 9'

NumeriCAL Process Calculation

PRODUCT IDENTIFICATION | PROCESS DATA

z-Value: Reference Temp: Initial Temp: Temp Unit: °F Simple or Broken: S
Evaluation: Container Type: Container Dimension: Today:

Segments	1S	2S	3S	4S	5C	6C	7C	8C	9C
Duration (min)	3.00	3.00	3.00	74.50	2.00	10.00	10.00	5.00	30.00
RT Begin	70.00	200.00	235.00	250.00	250.00	240.00	200.00	140.00	70.00
RT End	200.00	235.00	250.00	250.00	240.00	200.00	140.00	70.00	70.00
jh or jc	1.91	1.91	1.91	1.91	1.56	1.56	1.56	1.56	1.56
fh, f2, f3 or fc	48.21	48.21	48.21	48.21	53.26	53.26	53.26	53.26	53.26
Elapsed Time	3.00	6.00	9.00	83.50	85.50	95.50	105.50	110.50	140.50
Retort Temp	200.00	235.00	250.00	250.00	240.00	200.00	140.00	70.00	70.00
Product Temp	90.00	90.18	91.95	243.34	243.78	243.07	231.59	220.56	120.36
Accum F Value	0.000	0.000	0.000	6.007	6.887	11.573	14.014	14.273	14.328

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Temperature Ramp Increase

CUT	Hold Time	Total Heating
12'	72.67'	84.67'
9'	74.5'	83.5'

By creating a more aggressive come-up profile, the cycle time can be reduced 1.17' in this example.

Optimization Focus: Cooling

Cooling water temperature has the greatest impact on the ability to optimize the cooling profile in water spray retorts.

The colder the water, the more aggressive the cooling profile can be.

Optimization Focus: Cooling

There are several ways to improve the cooling profile:

1. Establish multiple “recipes” for retort operation that take into account cooling water temperature throughout the year.
2. Increase the exposed surface area in heat exchangers
3. Circulate cooling water through cooling towers.
4. Incorporate chillers on the cooling water infeed line.

Optimization Focus: Cooling

The following example demonstrates how we can reduce the cycle time by using colder water to achieve container center temperatures of 120° at the end of the process.

Typical Cooling Profile

Cooling Water Temperature = 70°F

NumeriCAL Process Calculation

PRODUCT IDENTIFICATION | PROCESS DATA

z-Value: Reference Temp: Initial Temp: Temp Unit: °F Simple or Broken: S
 Evaluation: Container Type: Container Dimension: Today:

Segments	1S	2S	3S	4S	5C	6C	7C	8C	9C
Duration (min)	4.00	4.00	4.00	72.67	2.00	10.00	10.00	5.00	30.00
RT Begin	70.00	200.00	235.00	250.00	250.00	240.00	200.00	140.00	70.00
RT End	200.00	235.00	250.00	250.00	240.00	200.00	140.00	70.00	70.00
jh or jc	1.91	1.91	1.91	1.91	1.56	1.56	1.56	1.56	1.56
fh, f2, f3 or fc	48.21	48.21	48.21	48.21	53.26	53.26	53.26	53.26	53.26
Elapsed Time	4.00	8.00	12.00	84.67	86.67	96.67	106.67	111.67	141.67
Retort Temp	200.00	235.00	250.00	250.00	240.00	200.00	140.00	70.00	70.00
Product Temp	90.00	90.72	95.65	243.37	243.82	243.09	231.61	220.57	120.37
Accum F Value	0.000	0.000	0.000	6.060	6.944	11.648	14.097	14.356	14.412

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OK Cancel Apply

Cooling Profile with Cooling Water Temperature = 50°F

NumeriCAL Process Calculation

PRODUCT IDENTIFICATION | PROCESS DATA

z-Value: 18 Reference Temp: 250 Initial Temp: 90 Temp Unit: °F Simple or Broken: S
Evaluation: 2-25-2009 Container Type: Container Dimension: Today: 2/25/20

Segments	1S	2S	3S	4S	5C	6C	7C	8C	9C
Duration (min)	4.00	4.00	4.00	72.67	2.00	10.00	10.00	5.00	25.50
RT Begin	70.00	200.00	235.00	250.00	250.00	240.00	200.00	140.00	50.00
RT End	200.00	235.00	250.00	250.00	240.00	200.00	140.00	50.00	50.00
jh or jc	1.91	1.91	1.91	1.91	1.56	1.56	1.56	1.56	1.56
fh, f2, f3 or fc	48.21	48.21	48.21	48.21	53.26	53.26	53.26	53.26	53.26
Elapsed Time	4.00	8.00	12.00	84.67	86.67	96.67	106.67	111.67	137.17
Retort Temp	200.00	235.00	250.00	250.00	240.00	200.00	140.00	50.00	50.00
Product Temp	90.00	90.72	95.65	243.37	243.82	243.09	231.61	220.51	120.33
Accum F Value	0.000	0.000	0.000	6.060	6.944	11.648	14.097	14.356	14.409

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Effect of Cooling Water Temperature Reduction

Cooling Water Temperature	Total Cooling Time
70°F	57'
50°F	52.5'

Without modifying the cooling ramp profile, we can realize a 4.5' reduction in cycle time by lowering the cooling water temperature by 20°F.

Optimization Focus: Cooling

Based on the capability of the retort, there may be more opportunities to reduce the cooling time through more aggressive cooling ramp steps.

Testing in the plant is necessary to determine just how aggressive the cooling ramp can be.

F-value at the End of Heating

One other salvo in our arsenal for optimizing thermal processes rests with our risk tolerance position. Targeting a lower F-value at the end of heating can also reduce cycle time.

Considerations for Reducing Target F-value at the End of Heating

- Confidence in the maintenance of machinery
- Ability to control critical factors upstream of the retort
- Confidence in the heating rate of the product determined through HP tests
- Company's risk tolerance position

Effect of Reducing End of Heating F-value

Provided there is confidence that the previously mentioned considerations have been addressed, the following example demonstrates the amount of time that can be reduced from a cycle by reducing the end of heating F_0 to 3.0' from 6.0':

Starting Process

$F_0 = 6.0'$ at end of heating

NumeriCAL Process Calculation

PRODUCT IDENTIFICATION | PROCESS DATA

z-Value: Reference Temp: Initial Temp: Temp Unit: Simple or Broken:
 Evaluation: Container Type: Container Dimension: Today:

Segments	1S	2S	3S	4S	5C	6C	7C	8C	9C
Duration (min)	4.00	4.00	4.00	72.67	2.00	10.00	10.00	5.00	30.00
RT Begin	70.00	200.00	235.00	250.00	250.00	240.00	200.00	140.00	70.00
RT End	200.00	235.00	250.00	250.00	240.00	200.00	140.00	70.00	70.00
jh or jc	1.91	1.91	1.91	1.91	1.56	1.56	1.56	1.56	1.56
fh, f2, f3 or fc	48.21	48.21	48.21	48.21	53.26	53.26	53.26	53.26	53.26
Elapsed Time	4.00	8.00	12.00	84.67	86.67	96.67	106.67	111.67	141.67
Retort Temp	200.00	235.00	250.00	250.00	240.00	200.00	140.00	70.00	70.00
Product Temp	90.00	90.72	95.65	243.37	243.82	243.09	231.61	220.57	120.37
Accum F Value	0.000	0.000	0.000	6.060	6.944	11.648	14.097	14.356	14.412

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OK Cancel Apply

Revised Process

$F_0 = 3.0'$ at end of heating

NumeriCAL Process Calculation

PRODUCT IDENTIFICATION | PROCESS DATA

z-Value: 18 Reference Temp: 250 Initial Temp: 90 Temp Unit: °F Simple or Broken: S
Evaluation: 2-20-2009 Container Type: Container Dimension: Today: 2/20/20

Segments	1S	2S	3S	4S	5C	6C	7C	8C	9C
Duration (min)	4.00	4.00	4.00	64.17	2.00	10.00	10.00	5.00	30.00
RT Begin	70.00	200.00	235.00	250.00	250.00	240.00	200.00	140.00	70.00
RT End	200.00	235.00	250.00	250.00	240.00	200.00	140.00	70.00	70.00
jh or jc	1.91	1.91	1.91	1.91	1.56	1.56	1.56	1.56	1.56
fh, f2, f3 or fc	48.21	48.21	48.21	48.21	53.26	53.26	53.26	53.26	53.26
Elapsed Time	4.00	8.00	12.00	76.17	78.17	88.17	98.17	103.17	133.17
Retort Temp	200.00	235.00	250.00	250.00	240.00	200.00	140.00	70.00	70.00
Product Temp	90.00	90.72	95.65	240.09	240.75	240.89	229.96	219.13	119.54
Accum F Value	0.000	0.000	0.000	3.033	3.623	6.996	8.901	9.114	9.161

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OK Cancel Apply

Effect of Reducing End of Heating F-value

End of Heating F_0	Process 'Hold' Time
6.0'	72.67'
3.0'	64.17'

By reducing the target F-value at the end of heating, an 8.5' reduction in heating time could be realized on each cycle. The downside is that the amount of extra lethality is also reduced, thus providing less cushion, should there be a process deviation.

Optimized Process

So how much cycle time can be claimed if we optimize the come-up, end of heating F-value, and cooling water temperature?

Let's take a look at the original process compared to a process with improved come-up, that delivers $F_0 = 6.0'$ at the end of the second cooling step and a final container center temperature of 120°F

Original Process

NumeriCAL Process Calculation

PRODUCT IDENTIFICATION | PROCESS DATA

z-Value: Reference Temp: Initial Temp: Temp Unit: Simple or Broken:
 Evaluation: Container Type: Container Dimension: Today:

Segments	1S	2S	3S	4S	5C	6C	7C	8C	9C
Duration (min)	4.00	4.00	4.00	72.67	2.00	10.00	10.00	5.00	30.00
RT Begin	70.00	200.00	235.00	250.00	250.00	240.00	200.00	140.00	70.00
RT End	200.00	235.00	250.00	250.00	240.00	200.00	140.00	70.00	70.00
jh or jc	1.91	1.91	1.91	1.91	1.56	1.56	1.56	1.56	1.56
fh, f2, f3 or fc	48.21	48.21	48.21	48.21	53.26	53.26	53.26	53.26	53.26
Elapsed Time	4.00	8.00	12.00	84.67	86.67	96.67	106.67	111.67	141.67
Retort Temp	200.00	235.00	250.00	250.00	240.00	200.00	140.00	70.00	70.00
Product Temp	90.00	90.72	95.65	243.37	243.82	243.09	231.61	220.57	120.37
Accum F Value	0.000	0.000	0.000	6.060	6.944	11.648	14.097	14.356	14.412

Spread Clear Import Print Evaluate tp calc

OK Cancel Apply

Optimized Process

NumeriCAL Process Calculation

PRODUCT IDENTIFICATION | PROCESS DATA

z-Value: Reference Temp: Initial Temp: Temp Unit: °F Simple or Broken: S
Evaluation: Container Type: Container Dimension: Today:

Segments	1S	2S	3S	4S	5C	6C	7C	8C	9C
Duration (min)	3.00	3.00	3.00	64.17	2.00	10.00	10.00	5.00	25.00
RT Begin	70.00	200.00	235.00	250.00	250.00	240.00	200.00	140.00	50.00
RT End	200.00	235.00	250.00	250.00	240.00	200.00	140.00	50.00	50.00
jh or jc	1.91	1.91	1.91	1.91	1.56	1.56	1.56	1.56	1.56
fh, f2, f3 or fc	48.21	48.21	48.21	48.21	53.26	53.26	53.26	53.26	53.26
Elapsed Time	3.00	6.00	9.00	73.17	75.17	85.17	95.17	100.17	125.17
Retort Temp	200.00	235.00	250.00	250.00	240.00	200.00	140.00	50.00	50.00
Product Temp	90.00	90.18	91.95	239.13	239.86	240.24	229.48	218.64	120.70
Accum F Value	0.000	0.000	0.000	2.512	3.036	6.098	7.868	8.069	8.111

Spread Clear Import Print Evaluate tp calc

OK Cancel Apply

Total Cycle Time Comparison

Process	Heating	Cooling	Total Cycle
Original	84.67'	57'	141.67'
Optimized	73.17'	52'	125.17'

By optimizing the original process, we can realize a 16.5' or 11.65% reduction in cycle time. This equates to one extra cycle for every 9 cycles processed.

Proceed with Caution!

A few key points to keep in mind:

1. When optimizing, take small steps since container integrity must also be verified throughout the testing.
2. Overpressure ramps may also need to be modified.
3. Involve other disciplines in the optimization process. Going too far can easily create problems for Operations and QC personnel.

Thank You!



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