

IFTPS
5th European Conference
Sevilla, Spain



Torre Del Oro

Nestlé Research

Holding Tube Calculations

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October 2015

UHT Plant + Aseptic Tank + Aseptic Filling Machine



From an engineering point of view the **Holding Tube** is the simplest part ...

... but nevertheless the **Holding Tube** determines

the **microbiological food safety**
or **spoilage risk** on one hand,

and the **product quality**
on the other.



Awareness

1

Heat Expansion of the Product

2

Amount of Condensate (liquid, dir. heat.)

3

Rheology of Products, Flow Regime

4

Pressure Losses

5

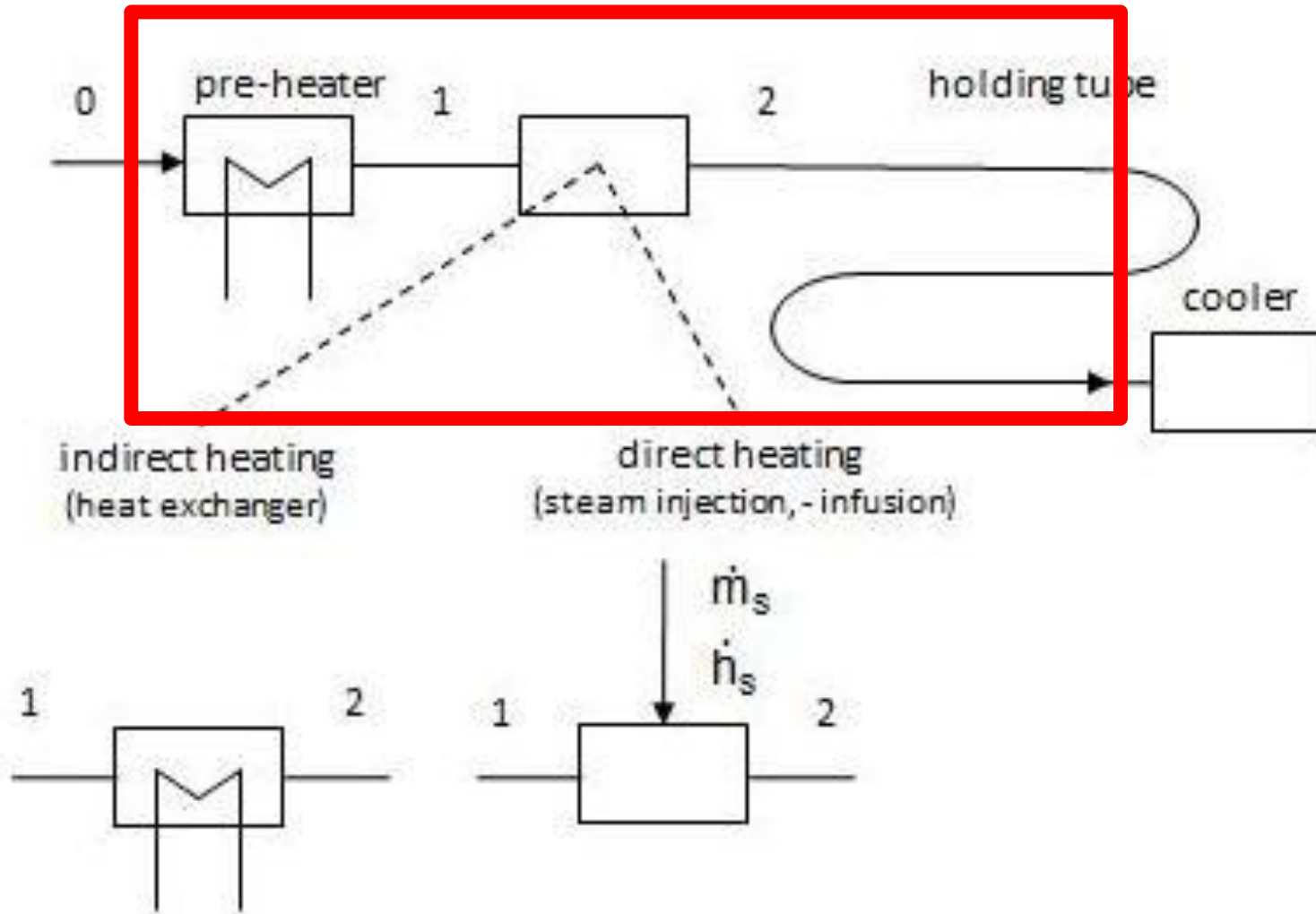
Residence Time Distribution

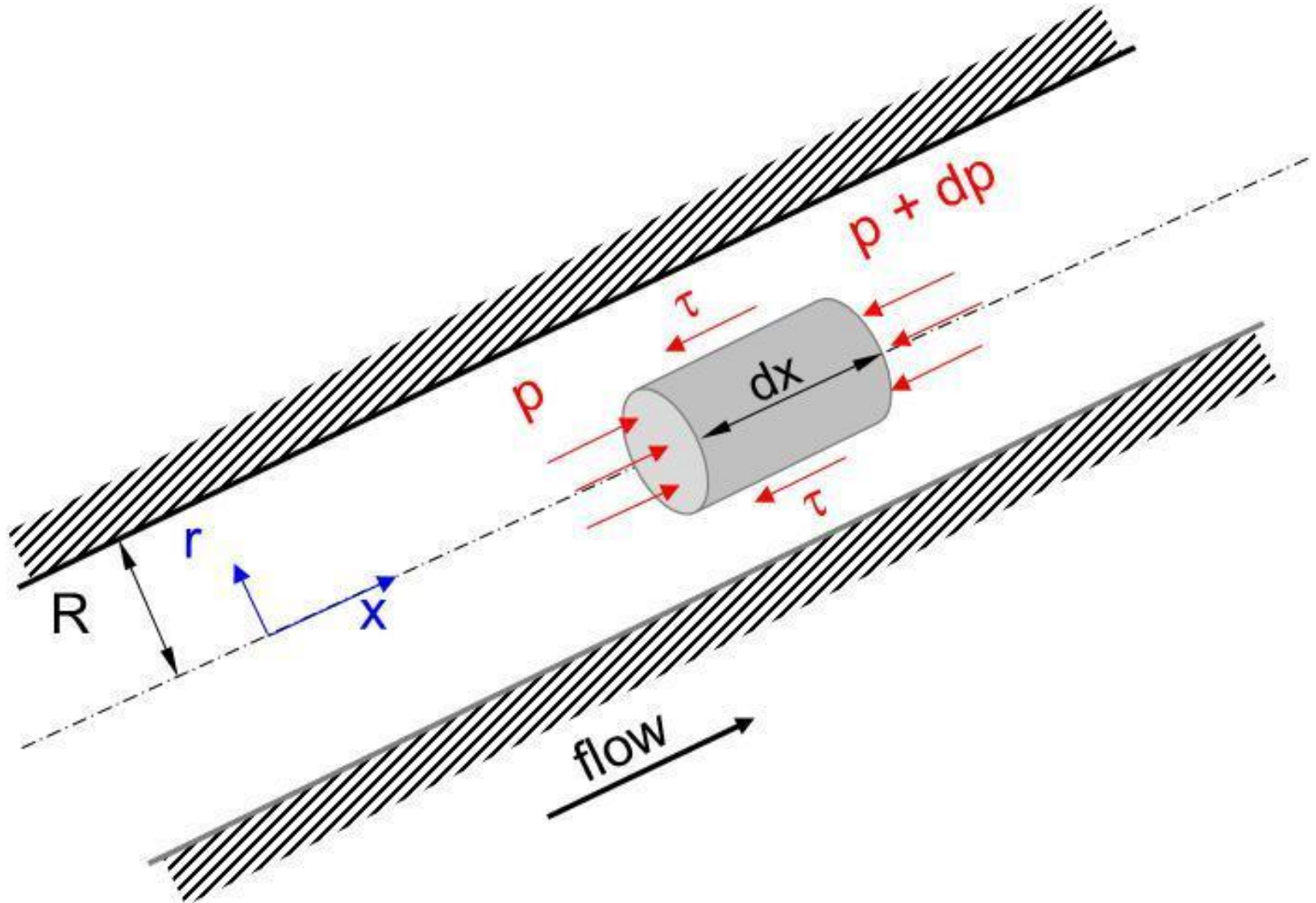
6

Fouling

7

Physical Properties

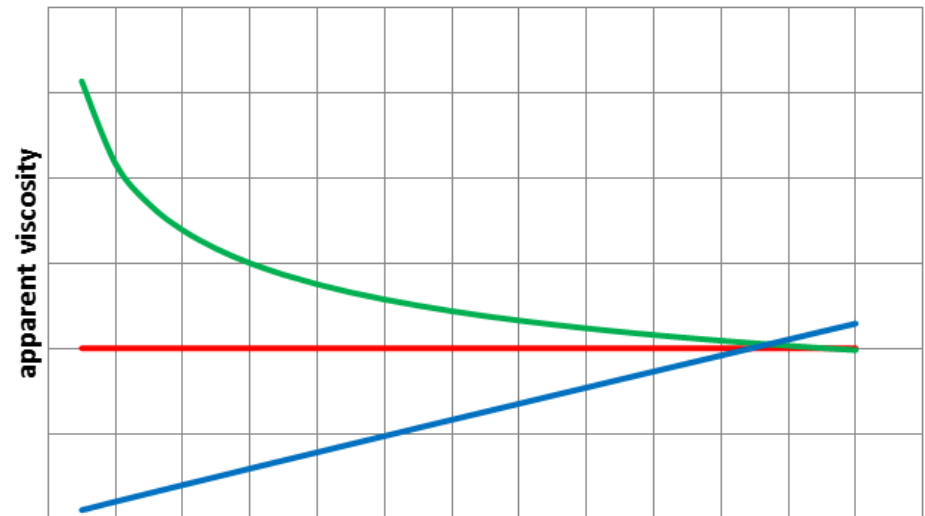




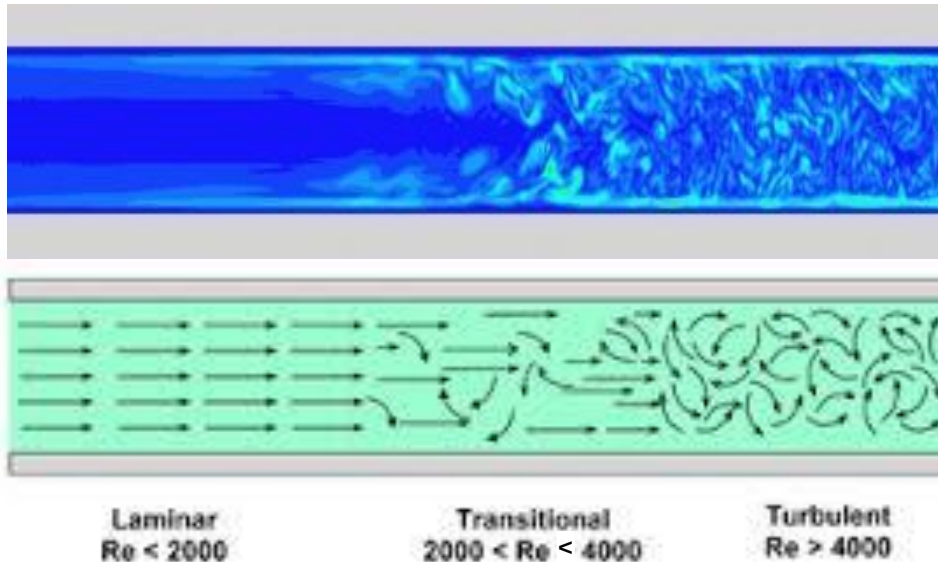
Power Law Liquids



n	liquid	example
$= 1$	<u>Newtonian</u>	water, fruit juice, skim milk, honey, vegetable oil
$0 < n < 1$	pseudoplastic, <u>shear-thinning</u> , (in German language: "strukturviskos")	applesauce, banana puree, orange juice concentrate
$1 < n < \infty$	dilatant, <u>shear-thickening</u>	some types of honey, 40% raw corn starch solution



— Newtonian, $n = 1$ — shear-thinning, $n < 1$ — shear-thickening, $n > 1$



$$\hat{u} = \frac{1}{C} \cdot \bar{u}$$

- For food safety reasons the maximum velocity must be considered.
- The average velocity is determined by the measured flow rate.
- The relation in between average and maximum velocity depends on the flow regime.

- The reverse correction coefficient $1/C$ is determined as follows:

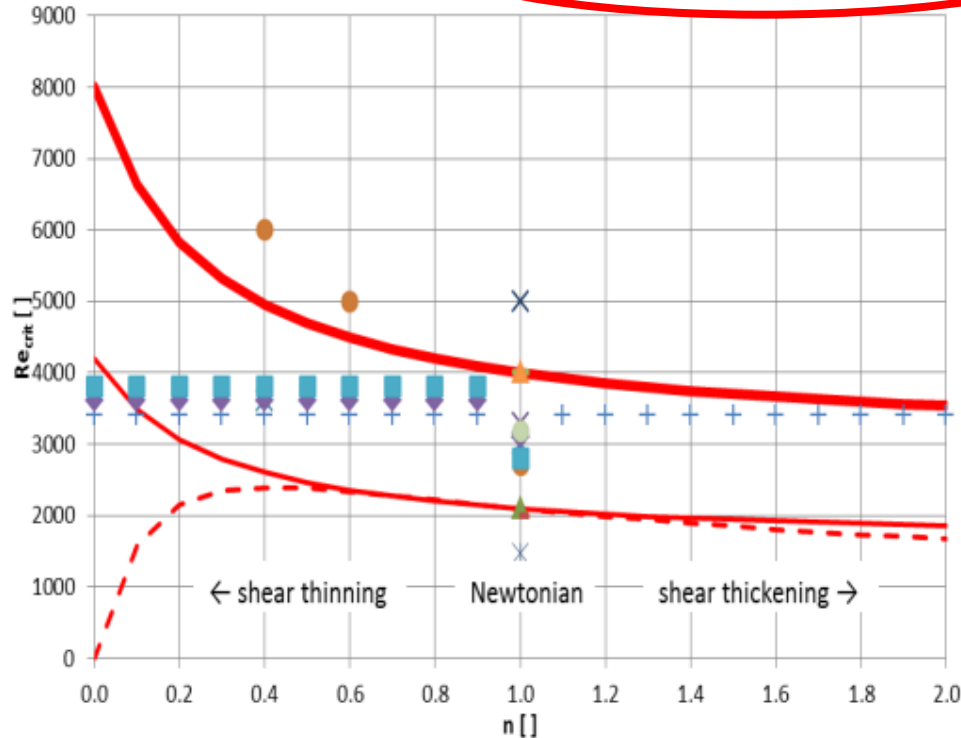
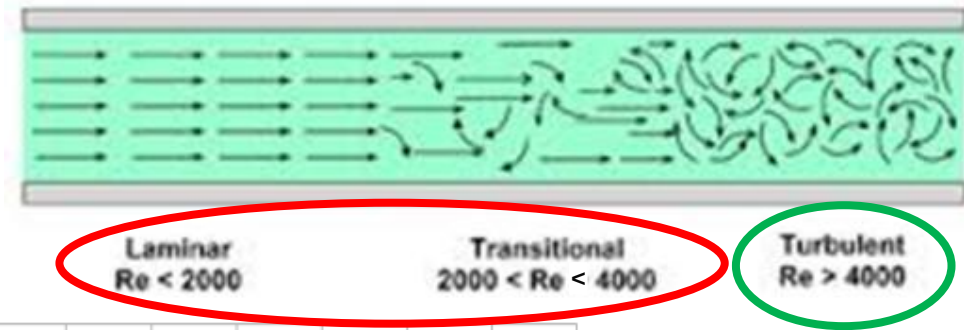
$1/C = 2$ for laminar flow (of Newtonian liquids)

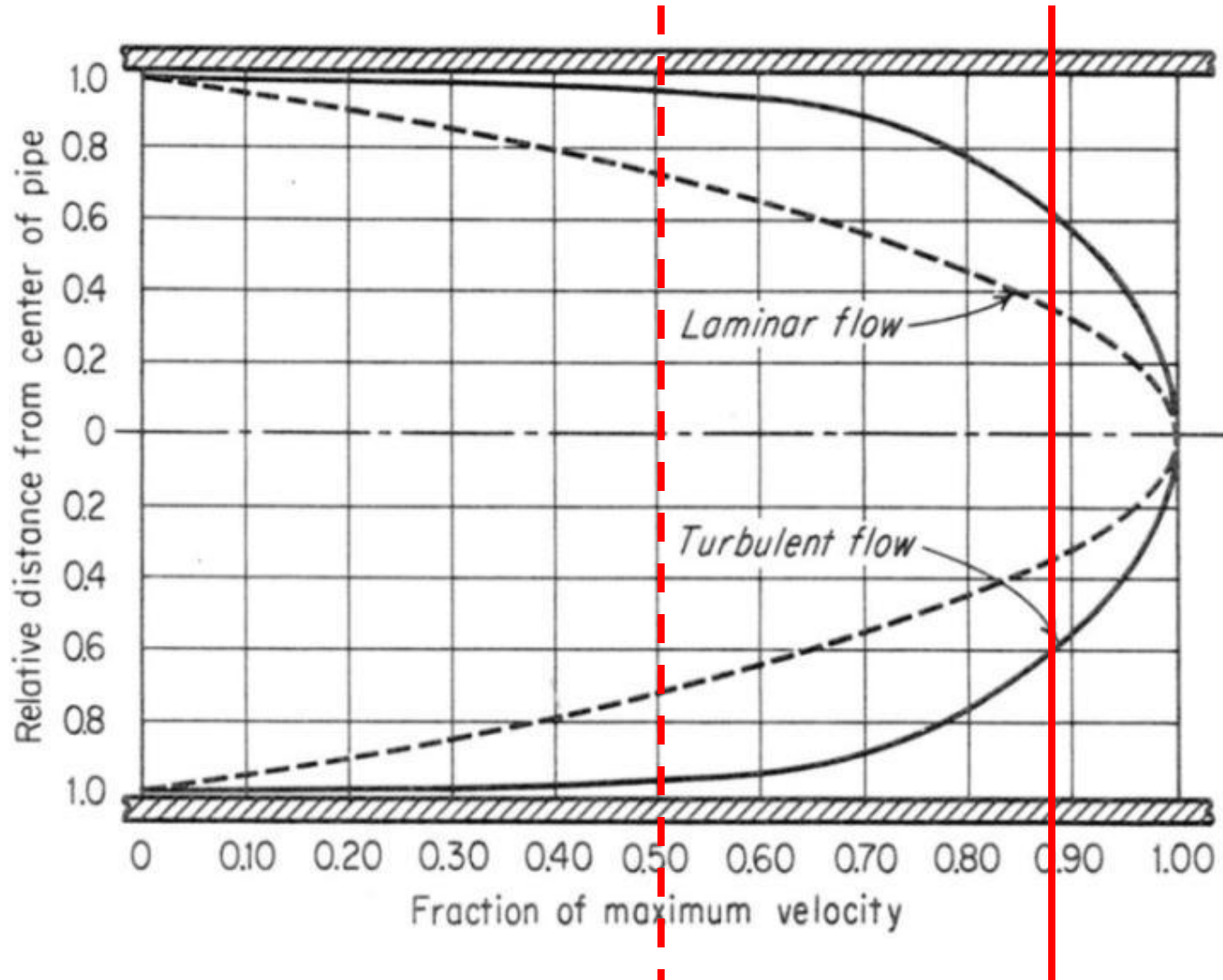
$1 < 1/C < 2$ for turbulent flow (of Newtonian liquids).

Reynolds Number for Power Law Liquids

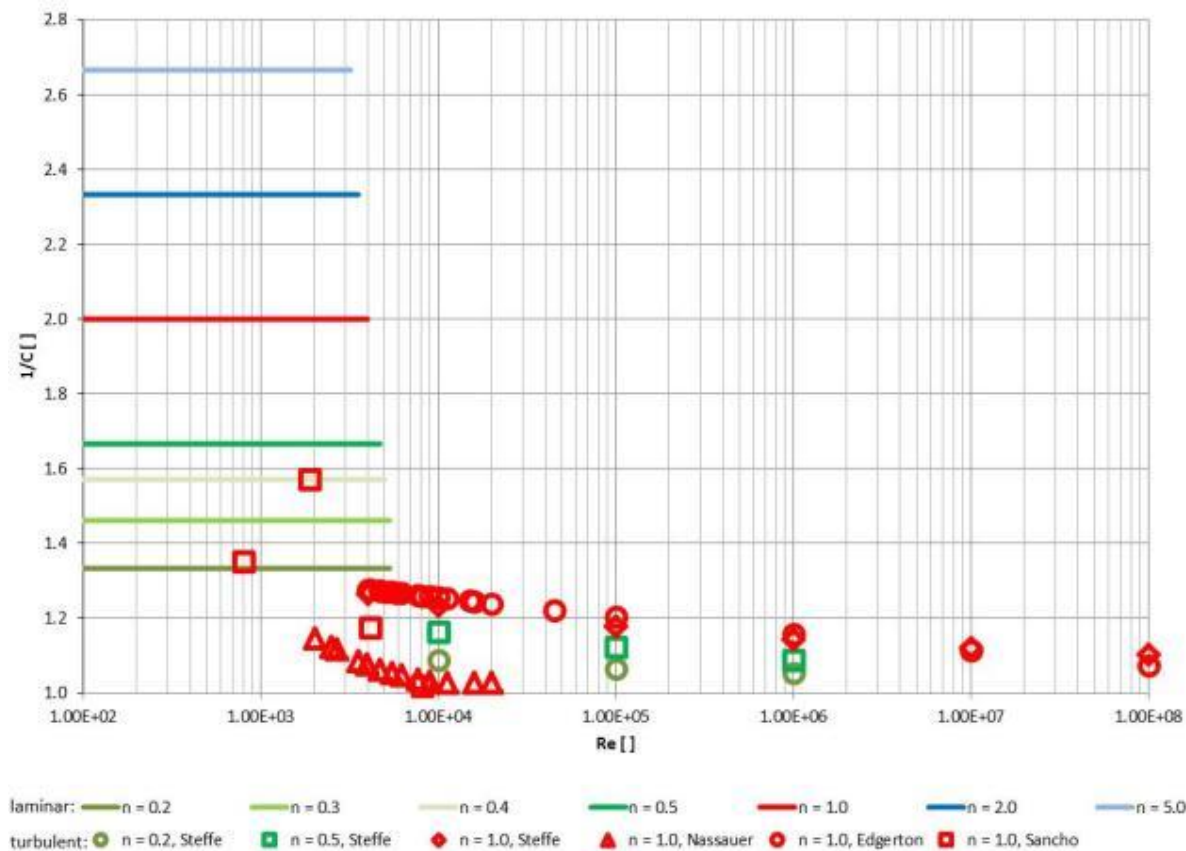
$$Re = \frac{2^n \cdot R^n \cdot \dot{\gamma}^{2-n} \cdot \rho}{8^{n-1} \cdot K} \cdot \left(\frac{4n}{3n+1} \right)^n$$

$$Re_{crit} = \frac{4000 \cdot (n+2) \cdot (n+3)}{3 \cdot (3n+1)}$$





$$\hat{u} = \frac{1}{C} \cdot \bar{u}$$



with n as flow behavior index: $0 < n < 1$: shear-thinning liquid
 $n = 1$: Newtonian liquid
 $1 < n < \infty$: shear-thickening liquid

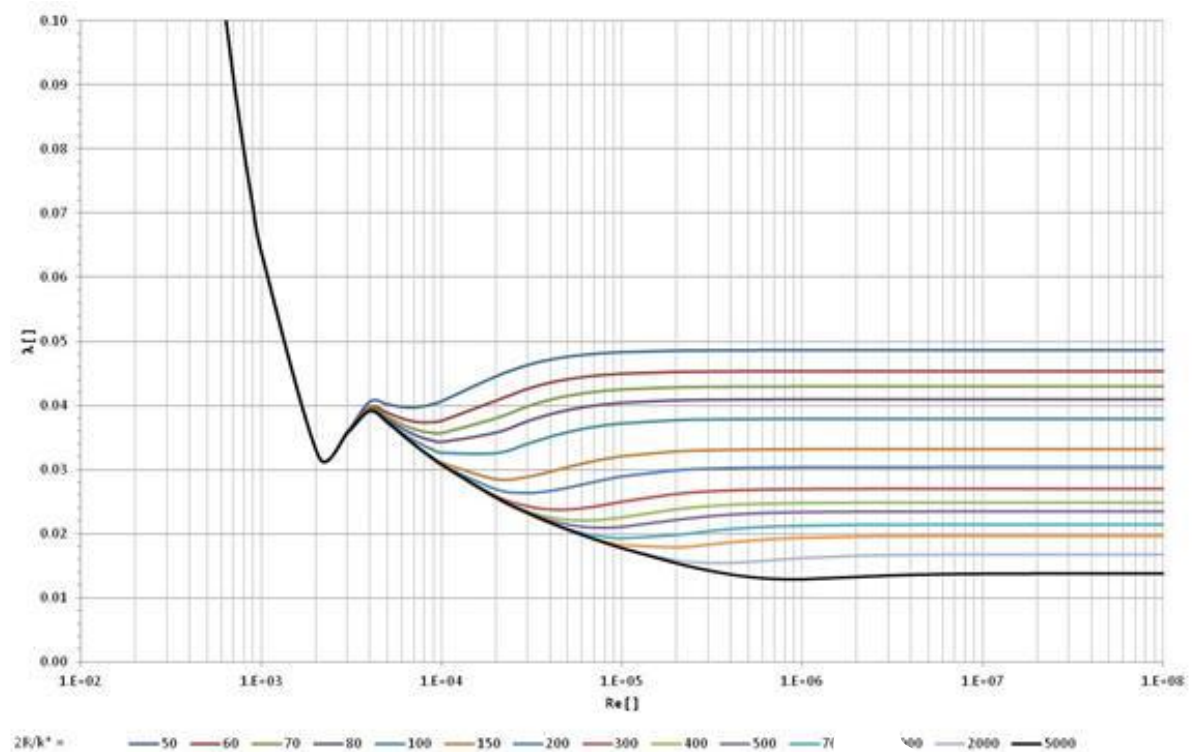
Figure 10 is a log-log plot showing the relationship between the inverse of the friction factor, $1/f$, and the Reynolds number, Re . The y-axis, labeled $1/f$ [], ranges from 1.0 to 2.8. The x-axis, labeled Re [], ranges from $1.00E+02$ to $1.00E+08$. The plot is divided into two regions: laminar flow (left) and turbulent flow (right). In the laminar region, $1/f$ is constant for each value of n . In the turbulent region, $1/f$ is constant for Newtonian and shear-thinning liquids ($n = 0.2$ to 0.5) and decreases for shear-thickening liquids ($n = 1.0$ to 5.0). The legend indicates that the lines represent different values of n and the flow regime.

Flow Regime	n	$1/f$ (approx.)
Laminar	0.2	1.34
	0.3	1.46
	0.4	1.57
	0.5	1.67
	1.0	2.00
	2.0	2.34
Turbulent	0.2 to 0.5	1.18
	1.0	1.05
	2.0	1.18
	5.0	2.67

1. Turbulent flow for Newtonian and shear-thinning liquids ($0 < n \leq 1$):

2. Turbulent flow for water and milk ($n = 1$, skim milk and whole milk):

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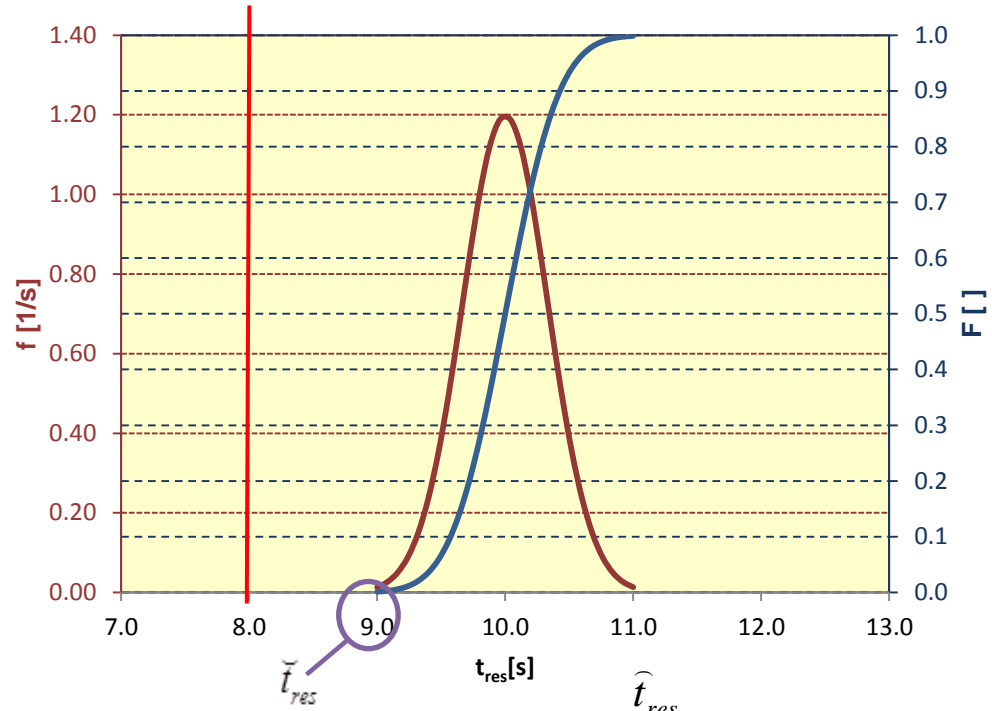
$$\bar{p}_{2abs} = \Delta p_{tube} + \Delta p_{fitt} + p_{boil,abs} + \underbrace{2 \text{ bar}}_{\text{experimental by PTC Konolfingen}}$$

$$\Delta p_{tube} = \lambda \cdot \frac{l}{2 \cdot R} \cdot \frac{\rho}{2} \cdot \bar{u}_L^2$$

$$f(t_{\text{res}}) = \frac{1}{\sqrt{2\pi}\sigma} e^{-\frac{1}{2}\left(\frac{t_{\text{res}} - \mu}{\sigma}\right)^2}$$

$$\mu = \bar{t}_{\text{res}} = \frac{1}{\bar{u}}$$

$$\sigma = \frac{1}{3} \cdot (\bar{t}_{\text{res}} - \check{t}_{\text{res}}) = \frac{1}{3} \cdot \left(\frac{1}{\bar{u}} - \frac{1}{\check{u}} \right)$$



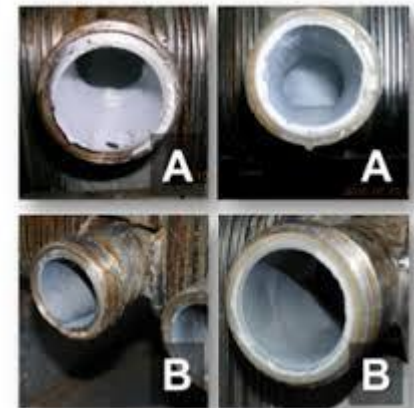
microbiological food safety
or **spoilage risk** ➔

product quality ➔

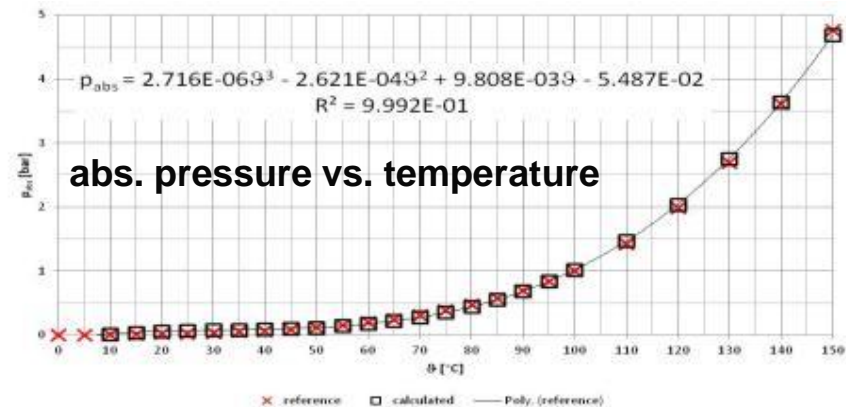
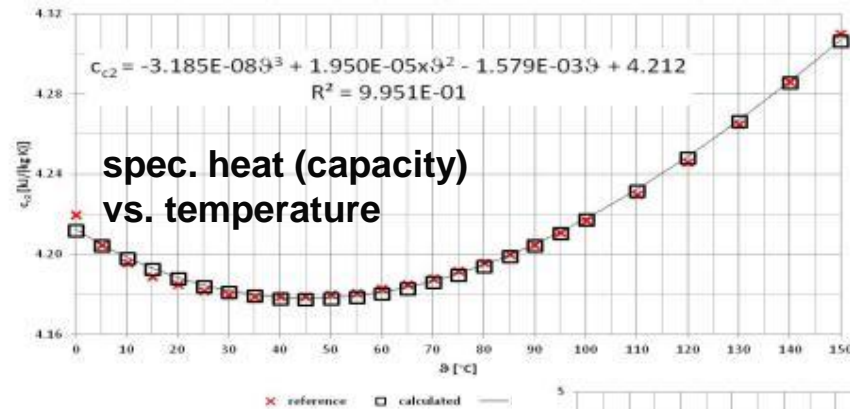
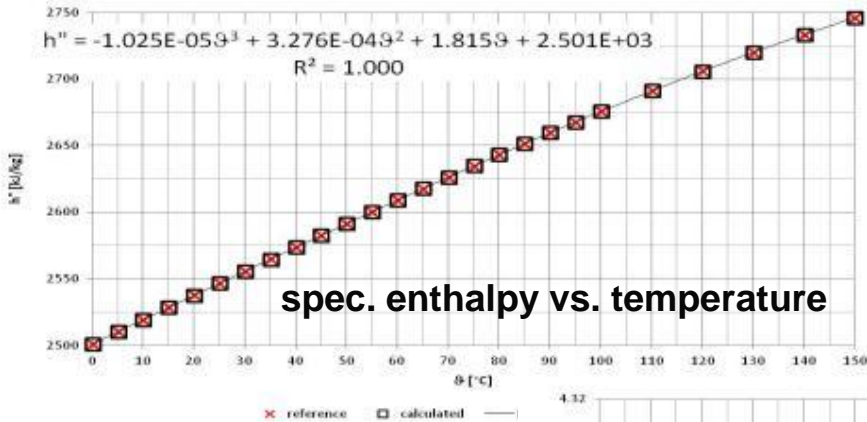
Here the composition of a constant fouling layer over the total holding tube lengths is supposed as follows:

$$R = R_{\text{clean}} - \delta_{\text{fouling}}$$

R: inner radius of the holding tube
 R_{clean} : inner radius of the clean (unfouled) holding tube
 δ_{fouling} : thickness of the fouling layer

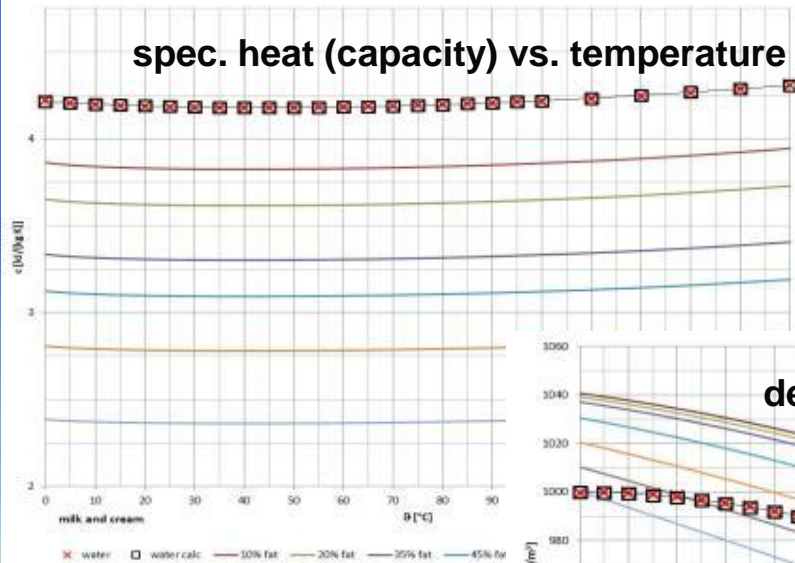


Physical Properties of Saturated Steam

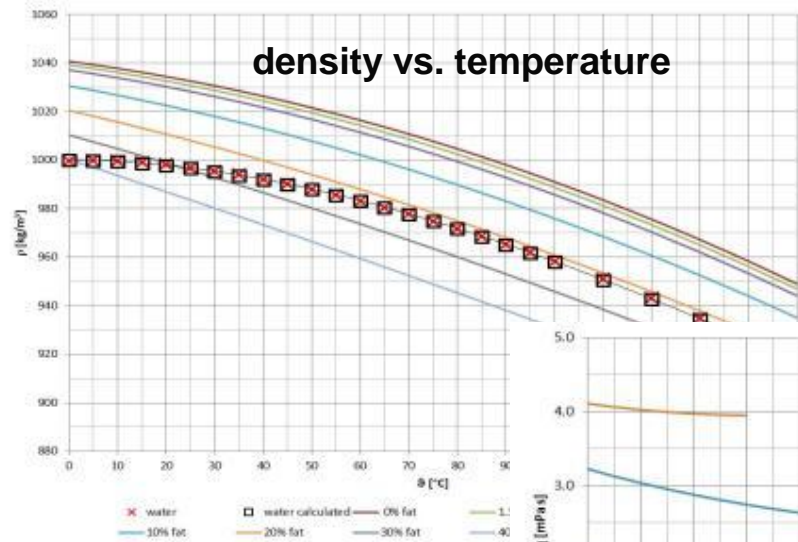


Physical Properties of Water, Milk, and Cream

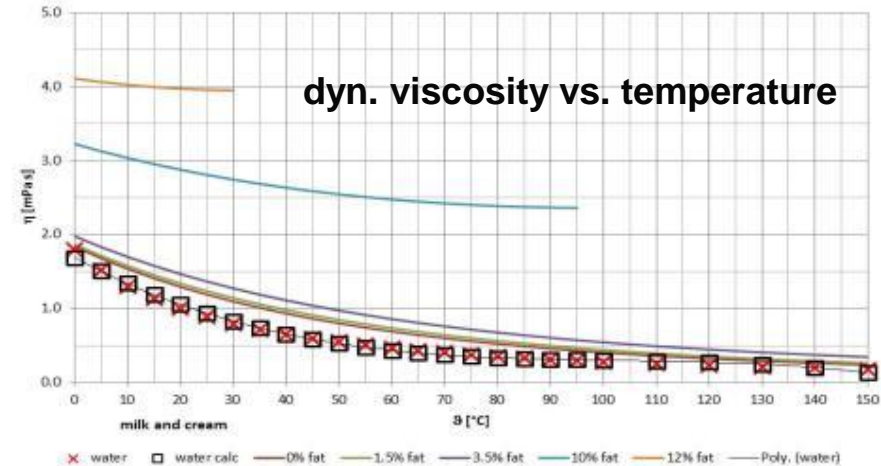
spec. heat (capacity) vs. temperature



density vs. temperature



dyn. viscosity vs. temperature



Validation / Qualification



New equipment design



product:	water	
(either or)	milk/cream \leq 12% fat	x
	any liquid product	
type of calculation:	lengths of the holding tube	
(either or)	residence time	x
type of heating:	direct	
(either or)	indirect	x

12 cases



Input

either
lengths of the holding tube

or
residence time in the holding tube

several input values
depending on the cases
(9 - 18 values)



Output

either
residence time in the holding tube

or
lengths of the holding tube

Reynolds Number,
minimum pressure,
width of the residence time distribution

9 - 18 input values

1. product temperature before pre-heater	ϑ_0	} always
2. product temperature after pre-heater	ϑ_1	
3. product temperature in holding tube	ϑ_2	
4. volume flow rate before pre-heater	V_0	
5. inner diameter of clean holding tube	$D_{\text{clean}2}$	
6. thickness of fouling layer	$\delta_{\text{fouling}2}$	
7. roughness at the inside of the holding tube	k_2^*	
8. number of 90° bends of the holding tube	$n_{\text{bend}2}$	
9. bend radius	$R_{\text{bend}2}$	
10. residence time in the holding tube	$t_{\text{res}2}$	} either / or
lengths of the holding tube	l_2	
11. product mass fraction of fat before pre-heater	x_{f0}	} milk/cream $\leq 12\%$ fat
12. product mass fraction of solids non fat before pre-heater	$x_{\text{snf}0}$	
13. product density before pre-heater	ρ_0	} any (other) liquid
14. product density before holding tube	ρ_2	
15. specific heat of the product in holding tube	c_2	
16. flow behavior index of the product in holding tube	n_2	
17. consistency coefficient of the product in the holding tube	K_2	
18. reverse correction coefficient	$1/C$	— confirmation



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THANK YOU

“Simplicity is the ultimate sophistication.”
(Leonardo da Vinci)